

Performance Optimization with Co-Feeds

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WWRFs can benefit by anaerobically digesting other organic materials

FACTS!

- More organic waste is becoming available due to organic waste bans
- Feed-in tariffs can be attractive for bio-based electricity
- More Co-Feeds = More biogas + tipping fees !!! = untapped revenues

Feedstocks	TS (%)	VS (%)	Tip Fee (typ)	\$/load (avg)	relative BMP
Sludge	5%	78%	n/a	n/a	1
Generic Food	13%	92%	\$20-\$50/ton	\$600 - \$800	2.2
FOG	4%	90%	10¢/gal	\$1,000	2.0
Dairy Processing	10%	70%	3¢ - 8¢/gal	\$500-\$600	1.7
<i>Relative BMP based on sludge = 300 Nm³ CH₄/ton VS</i>					

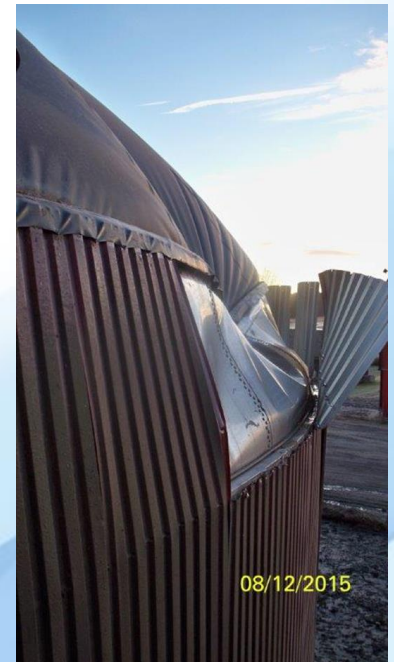
If you have excess capacity, then co-feeds are a smart addition.

Sources of extra revenue for WWTP

What are the barriers?

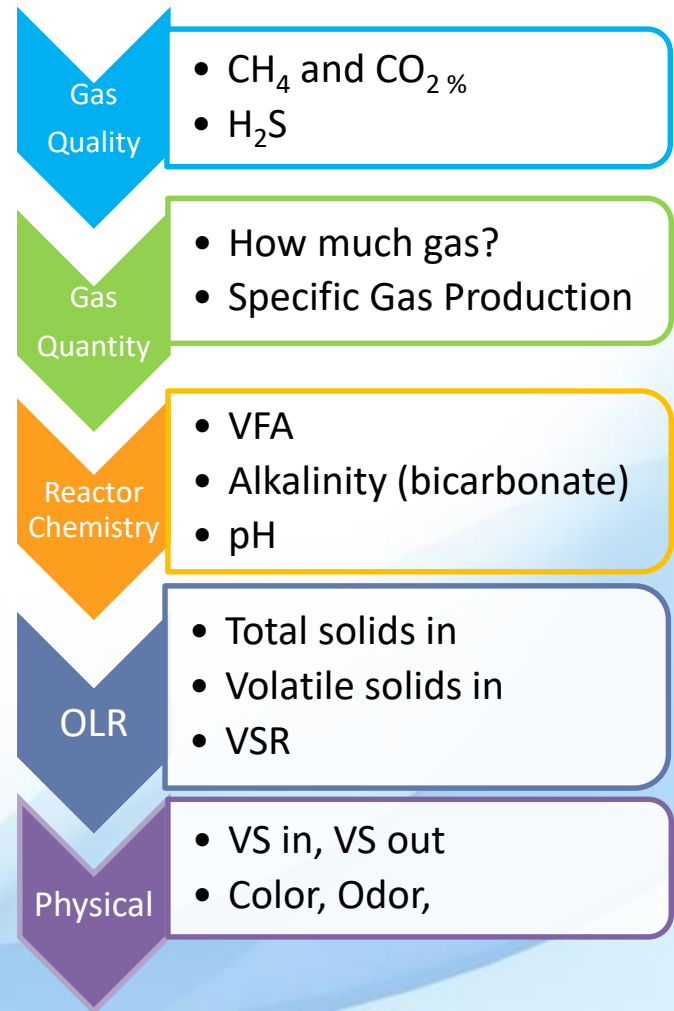
Co-feedstocks can deliver more revenue to the plant, BUT

- More biological activity requires better monitoring
- More biogas production - How do you capture the most value?
- Do you have the capacity to handle the increased biogas production?
- Co-feedstocks can result in biochemical imbalance



Monitoring digester biochemistry

- When accepting co-feedstocks, regular monitoring is essential.
- Key biochemical parameters tell the operator about current digester health.
- Future performance can also be predicted if the historical data is valued








Typical guidelines for a healthy AD

A stable and productive digester has:

- A pH between 6.8 –7.8
- Sufficient alkalinity
- Low volatile fatty acids (VFAs)
- No rapid changes in temperature
- No toxic/inhibitory compounds present in the influent
- Enough nutrients (N & P) and trace metals - esp. Fe, Co, Ni, etc.
- All key biochemical ratios within range

How does this change with co-feeds?

A digester with co-feedstocks:

- A pH between 6.8 –7.8  Caution is needed when taking high volumes of acid waste
- Sufficient alkalinity  May need to add buffering agent
- High volatile fatty acids (VFAs)  Can your AD handle the conversion of VFAs without buildup?
- Toxic/inhibitory compounds  Know how your feed stocks are generated!
- Adequate N, P and trace metals  Sewage sludge provides macro- and micro-nutrients... may need to augment

What you know today

HRT – Hydraulic Retention Time

= Retention time for feedstock in reactor vessel.

$$\text{HRT (days)} = \frac{\text{Reactor volume}}{\text{Daily feed rate}}$$

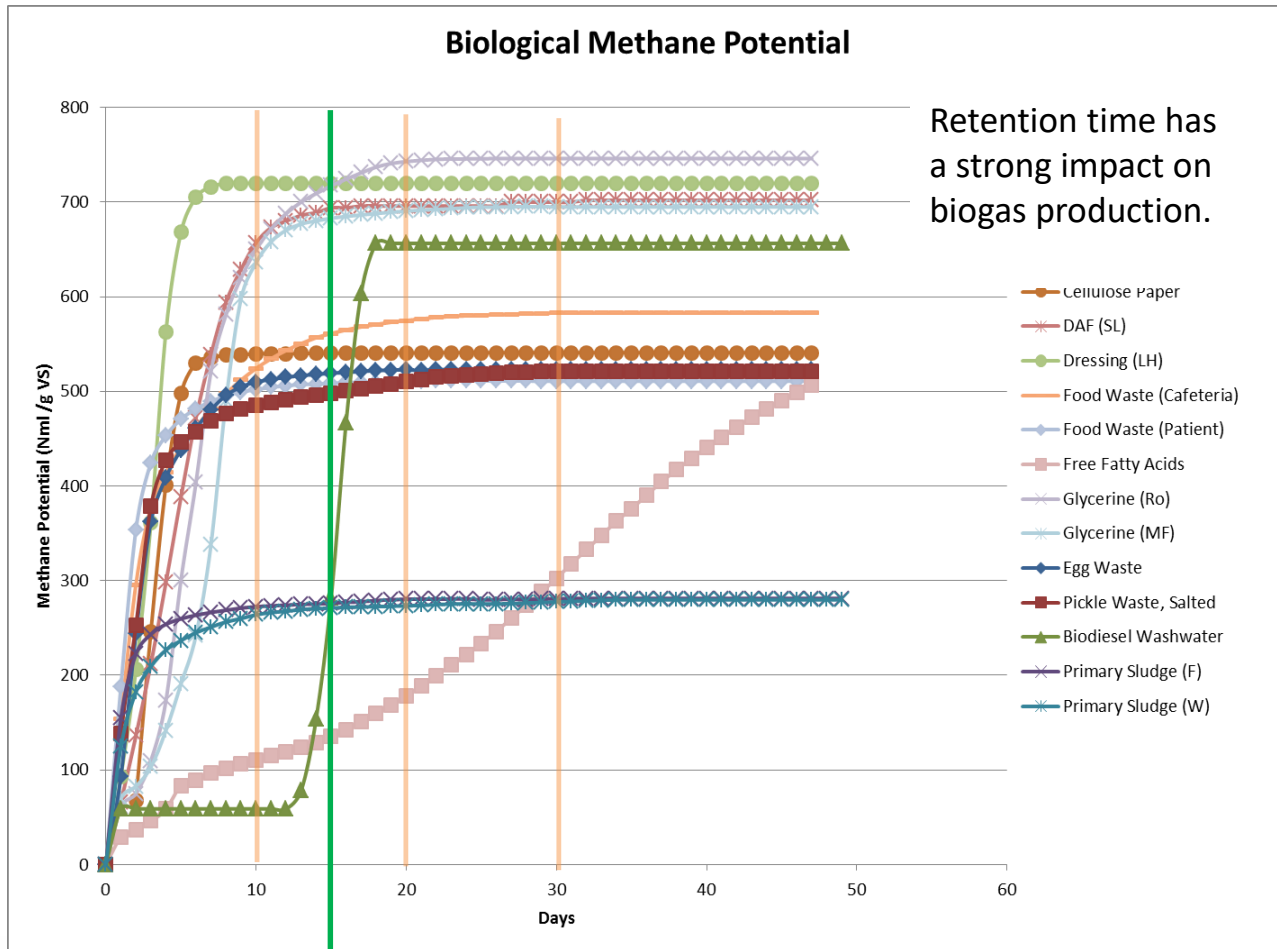
SRT – Sludge Retention Time

= Retention time for active biomass in the reactor vessel.

For most WWTP AD systems, HRT = SRT

Tracking of HRT is typically performed for Biosolids compliance

HRT/SRT



15 days - Class B

Note: Cellulosic materials will take longer to digest than sludge or manure.

Example of Mass Loading to Reactor

Inputs

- Feed Rate – 75,000 gpd
- Total solids – 5%
- Volatile Solids - 75% (VS of TS)



Mass Loading

- Total Solids = $75,000 \text{ gpd} \times 0.05 \times 8.34 \text{ lb/gal} = 31,275 \text{ lb/day}$
 $= 15.6 \text{ tons/day}$
- Volatile Solids = $0.75 \times 15.6 \text{ tons/day} = 12.5 \text{ tons/day}$

Example of Mass Loading to Reactor with co-feeds

Inputs

- Feed Rate of Co-feeds 30,000 gpd
- Total solids – 12%
- Volatile Solids - 83% (VS of TS)

Mass Loading

- Total Solids = $30,000 \text{ gpd} \times 0.12 \times 8.34 \text{ lb/gal}$
= 30,024 lbs/day
= 15 tons/day
- Volatile Solids = $0.83 \times 15 \text{ tons/day} = 12.46 \text{ tons/day}$



Large increase of solids loading to the reactor – do you have the biomass to stabilize?

Total Volatile Solids loading to Reactor

- A high/low feed rate can lead to poor performance
- The operator needs to carefully control the %VS/day added
- Total volatile solids (mass) will impact:
 - VFA/ALK ratio (a rapid change is undesirable)
 - OLR (depending on the organic content of the feedstock)
 - Volume of gas production
 - Volatile Solids Reduction

VFA/ALK Ratio

Ratio indicates the progress of digestion and stability

$$\text{VFA/ALK} = \frac{\text{Volatile Acids (mg/l)}}{\text{Alkalinity (mg/l)}}$$

The healthy range of VFA/ALK is 0.1 to 0.35

If AD is becoming unstable, the VFA/ALK ratio will begin to trend above 0.25.

VFA/ALK = 0.35, Warning

VFA/ALK = 0.5, Sour digester (big problems)

Proper Ratio of VFA/ALK

We know:

- If the VFA/ALK begins to trend past 0.25, the operator can reduce total feed and monitor key metrics
- OR ... add alkaline materials to decrease VFA/ALK ratio
- As the VFA/ALK increases past a healthy range, CO_2 goes up and CH_4 production goes down.
- The pH of the digester will begin to decrease.

NOTE: The VFA/ALK ratio is highly dependent on OLR



Organic Loading Rate

$$\text{OLR} = \frac{\text{kg (or lbs) of Volatile Solids (VS)}}{\text{m}^3 \text{ (or ft}^3\text{) of the reactor}}$$

OLR is a design value for each digester, and varies from system to system (depending on design)....

For completely mixed systems

$$\begin{aligned}\text{OLR} &= 80 \text{ lbs-VS per } 1000 \text{ ft}^3 \text{ per day} \\ &= 1.3 \text{ kg-VS per m}^3 \text{ per day} \\ &\text{(typical per Ten States Standard)}\end{aligned}$$

HIGHER OLR = optimized use of reactor volume
.... to a point....

How high can you go???



OLR with multiple co-feeds

Managing OLR is critical when processing co-feeds. With several co-feeds, the OLR is **ADDITIVE**.

Example:

$$\text{OLR total} = \text{OLR sludge} + \text{OLR food waste} + \text{OLR FOG}$$

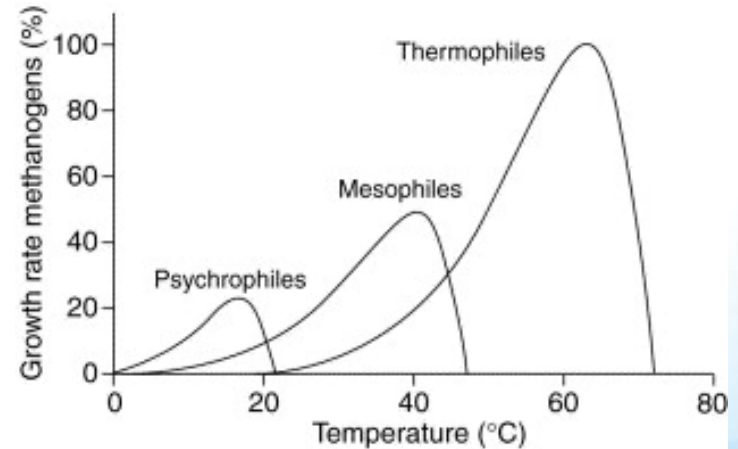
$$= \frac{\text{lbs-VS sludge} + \text{lbs-VS food waste} + \text{lbs-VS FOG}}{\text{Reactor Volume}/1000 \text{ ft}^3}$$

Note: OLR is normalized to each 1000 ft³ of reactor volume with units of units of lbs-VS/1000 ft³.

Temperature & Time

There is no absolute temperature requirement; rather, temperature ranges.

However, it is *critical* to limit ΔT to less than 1 deg C/day.



TRENDS in Biotechnology

Duration and Temperature are related:

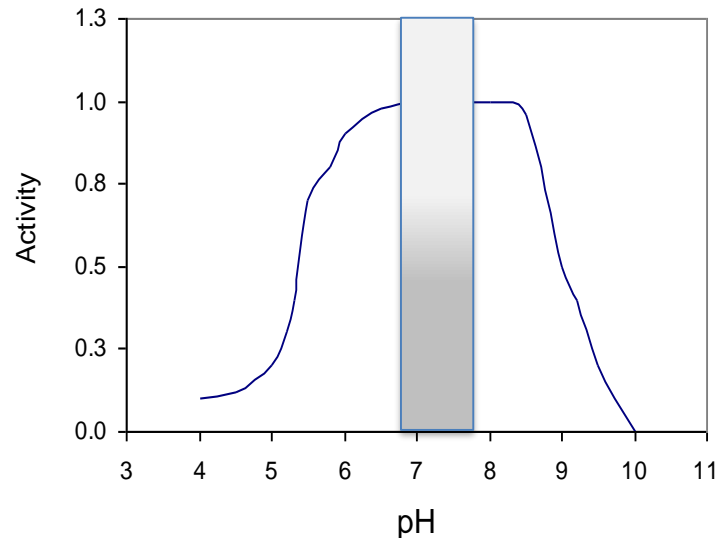
- Class B pathogen reduction: @ 95 F for 15 days
- Class A pathogen reduction: @122 F for 30 min (typ).

Caution: Self-heating of system can occur with high-carbohydrate co-feeds (... and, BTW, sewage is not a high carbo substrate)

pH

- A good operating pH is 6.8 to 7.8.
- A low pH reduces the activity of methanogens, resulting in an increase in VFA and H² production

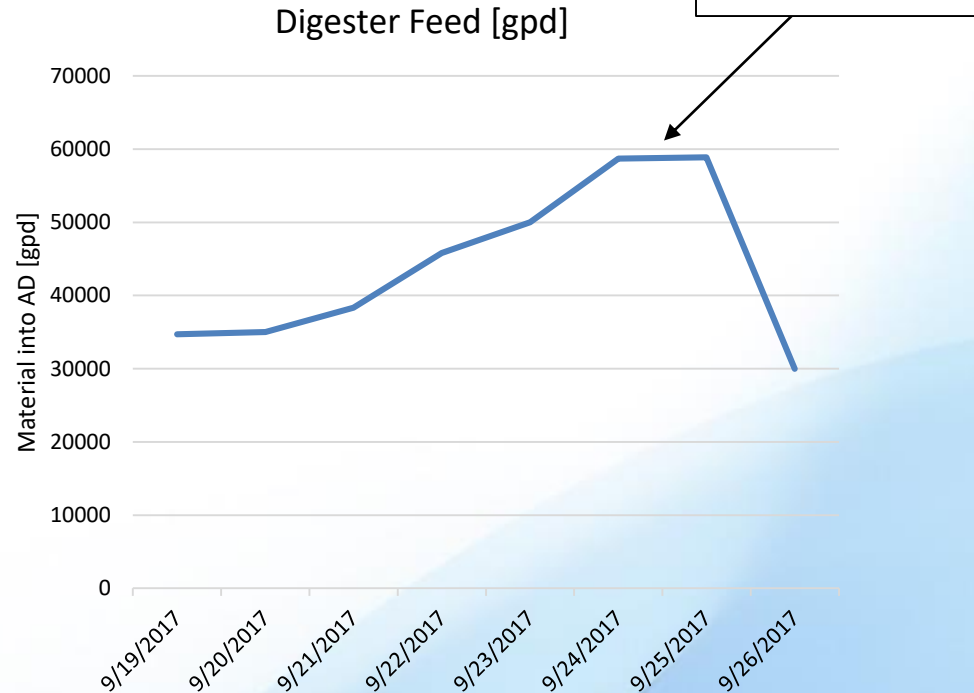
Relative activity of methanogens to pH



Depending on alkalinity concentration, pH reduction could be delayed. By the time pH is out-of-range, the digester has already “soured”.

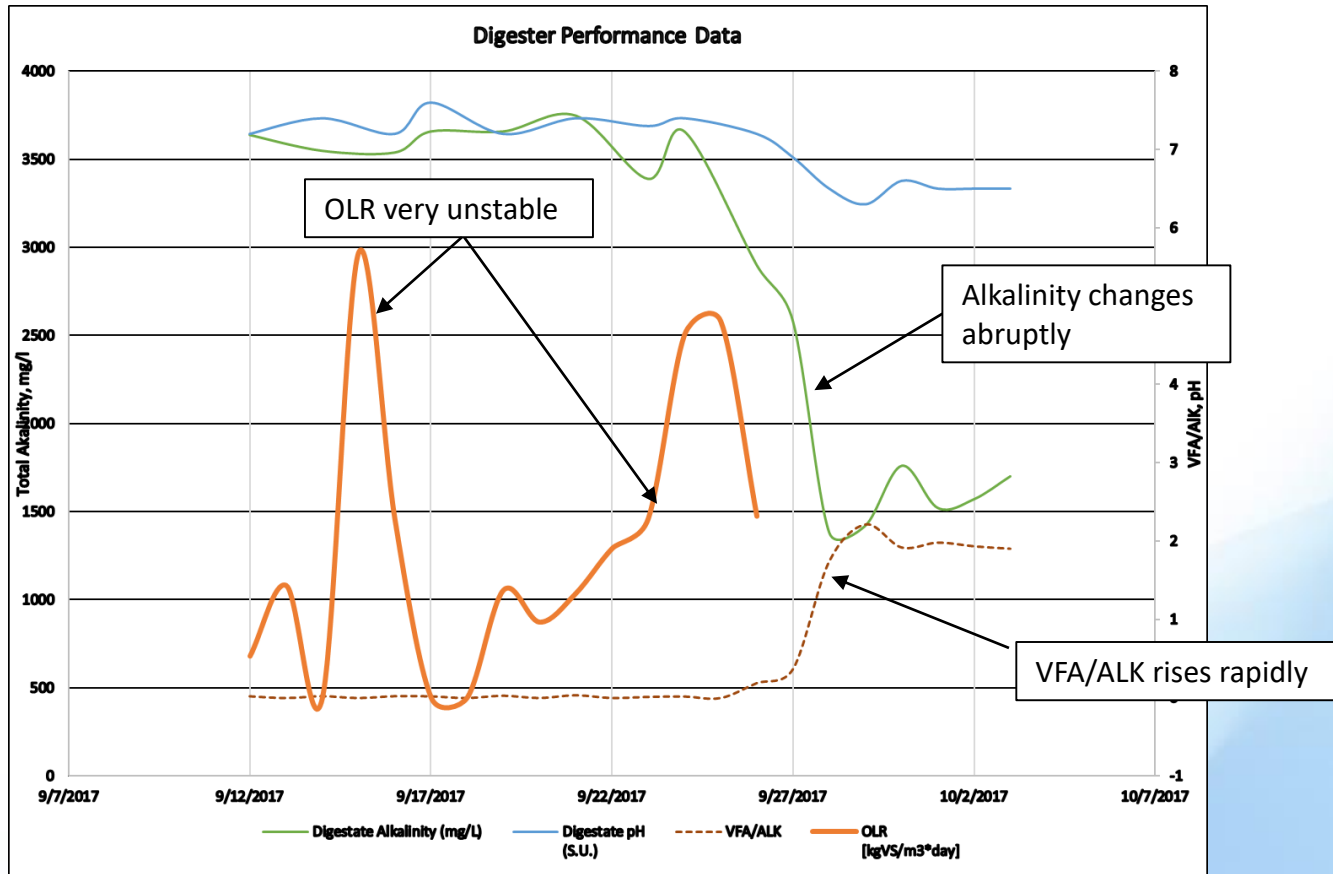
Step-wise approach to AD monitoring

- Gather data on key parameters over several days
- Monitor slow changes, react to abrupt changes
- Plot out individual parameter to visualize trends (and performance).



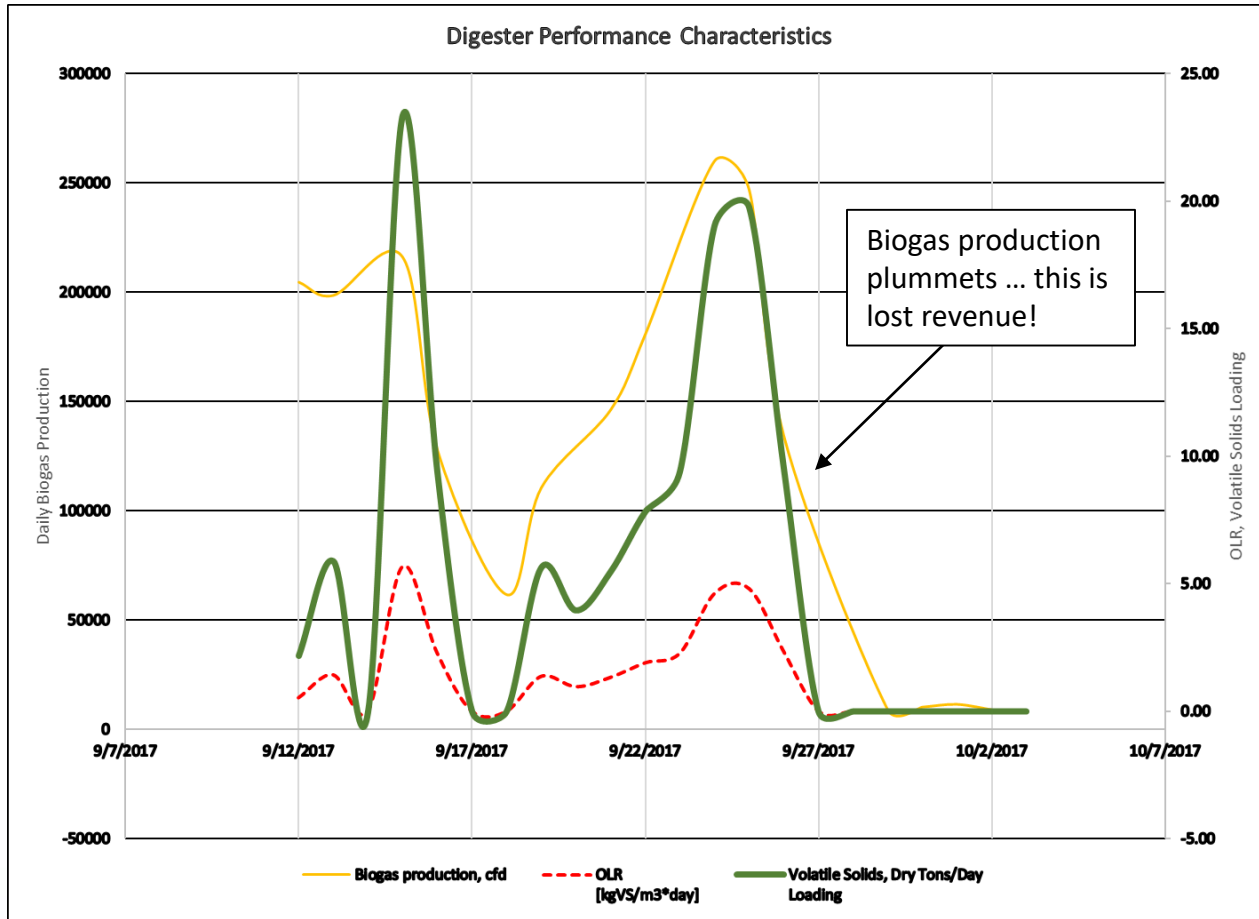
Example: Rapid changes to the AD feedrate

Resulting changes in key biochemical parameters



Track/evaluate data for alkalinity, pH, VFA/ALK and OLR

A substantial drop in AD performance



Biogas production is a measure of "value" to the plant's operation

Case Study: Co-Feeds at a WRRF

- The City of Flint Michigan and BioWorks Energy have a public-private partnership to digest co-feedstocks
- 50 MGD WRRF currently flowing ADF at 15 MGD
- Formerly used sludge incineration as disposal method
- BioWorks Energy developed private-public partnership – 21 year operating agreement
- Project co-digests food waste/byproducts along with WWTP sludges
- Why is this a successful partnership?
 - Each partner does what they do best; City operates, BioWorks provides service that the City is not configured to perform
 - Revenue from project benefits both partners

Case Study: Flint Biogas Plant

Physical Plant

- Two (2) 1.1 million gallon digesters
- One (1) 1.1 million gallon substrate storage tank
- 600 kW of electrical power generation capacity – and growing
- All power used onsite
- 35 to 50k gpd of co-settled sewage sludge
- 20 to 30k gpd of feedstocks

Ability to accept:

- Liquids
- Semi solids
- Packaged goods

*Successful Private – Public Partnership
A true Win-Win for both parties.*



List of Co-Feedstocks:

- FOG
- Sugar Waste
- Cucumber waste
- Milk waste
- Biodiesel byproduct
- Food waste

The most desirable co-feed is what pays the best 😊

Questions?



Feel free to ask or email us any follow-up questions!

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